Application No. 10/686,697 Paper Dated: March 30, 2009

In Reply to USPTO Correspondence of October 3, 2008

Attorney Docket No. 5219-061243

# IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Application No.

10/686,697

Confirmation No. 7668

Applicant

PAUL A. KOHL

Filed

October 16, 2003

Title

POLYMERS, METHODS OF USE THEREOF, AND

METHODS OF DECOMPOSITION THEREOF

Group Art Unit

1795

Examiner

Sin J. Lee

Customer No.

28289

Mail Stop Amendment Commissioner for Patents P. O. Box 1450 Alexandria, VA 22313-1450

## DECLARATION UNDER 37 CFR § 1.131 SHOWING CONCEPTION AND DILIGENCE PRIOR TO SEPTEMBER 13, 2002 UNTIL FILING

Sir:

- I, Paul A. Kohl, hereby declare as follows:
- 1. I along with SueAnn Bidstrup Allen, Xiaoqun Wu and Clifford Lee Henderson are the named inventors and assignees of the invention described and claimed in the above-captioned application. A copy of my curriculum vitae is included as Exhibit A.
- 2. As evidenced by the attached Exhibit B, the present invention was first conceived on July 24, 2000 (page 3) and later disclosed in an Invention Disclosure Form (IDF) provided by the Georgia Tech Research Corporation Office of Technology Transfer, which is dated February 12, 2001 (page 1). The Invention Disclosure Form was signed by two witnesses on February 7, 2001 (page 4). Please note that references to page numbering of Exhibit B correspond to the number located at the bottom right hand corner of each page.

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3. The IDF and accompanying figures are directed to a method of fabricating microchannels using polynorbornene photosensitive sacrificial materials. The materials describe the fabrication of the microchannels by the thermal decomposition of the sacrificial polymers, thus forming air channels. See pages 6, 19-20; Figure 1. The IDF describes the composition of the sacrificial polymer including the thermal decomposition characteristics (page 13; Figures 6 and 7); microchannel fabrication (pages 13-14) and the calculation of the thermal decomposition profile (pages 13-16). The results clearly describe the successful fabrication of microchannels. See pages 16-26; Figures 11-13.

- 4. From July 24, 2000 until February 12, 2001, we proceeded diligently to work on the development of the sacrificial polymer fabrication methods to produce channel geometries with arbitrary shaped cross-sectional profiles by developing channel geometries, synthesizing various sacrificial polymers, determining thermal decomposition characteristics and fabricating microchannels.
- 5. The present application claims the benefit of U.S. Provisional Patent Application No. 60/418,930, dated October 16, 2002, which is the effective filing date of the present application.
- 6. From February 12, 2001 until the United States effective filing date of October 16, 2002, the inventors prepared and finalized the figures, explained the invention to patent counsel and reviewed the patent application prepared by patent counsel.
- 7. The above utility application was subsequently filed in the United States Patent and Trademark Office on October 16, 2003, claiming the benefit of the corresponding U.S. Provisional Patent Application.
- 8. The aforementioned activities, from about July 2000 to August 2002 (Exhibit B), demonstrate the required evidence of conception prior to the effective date of the cited reference, i.e., September 13, 2002, as well as diligence and constructive reduction to practice of the present invention.

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9. I declare further that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true, and further that these statements are made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment or both, under Section 1001 of Title 18 of the United States Code, and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

Paul A. Kohl

3/30/2009 Date

# Paul A. Kohl Regents' Professor School of Chemical and Biomolecular Engineering

#### **EARNED DEGREES**

<u>Degree</u>	<u>Year</u>	<u>University</u>	<u>Field</u>
Ph.D.	1978	University of Texas at Austin	Chemistry
B.S.	1974	Bethany College	Chemistry

# **EMPLOYMENT**

<u>Title</u>	<u>Organization</u>	<u>Years</u>
Director, SRC Interconnect and Package	ging Center at Georgia Tech	2009-present
Hercules Inc./Thomas L. Gossage Cha	ir Georgia Tech	2006-present
Director, Interconnect Focus Center	MARCO Center homed at GT	2006-present
Regents' Professor	Georgia Tech	1999-present
Institute Fellow	Georgia Tech	1996
Professor	Georgia Tech	1994-1999
Associate Professor	Georgia Tech	1989-1994
Technical Supervisor	AT&T Bell Laboratories	1982-1989J
Member of Technical Staff	AT&T Bell Laboratories	1978-1982

# **HONORS AND AWARDS**

- 1. Analytical Chemistry Award from the American Chemical Society in 1973.
- 2. Awarded Academic Distinction in chemistry from Bethany College in 1974.
- 3. Gilbert H. Ayers for outstanding graduate work in chemistry in 1977.
- 4. Edward Weston Fellowship from the Electrochemical Society in 1977.
- 5 Named one of "America's 100 Brightest Scientists Under 40" by Science Digest in 1985.
- 6. Outstanding Alumni Achievement Award presented by Bethany College in 1986.
- 7. Outstanding Faculty Award, 1990-1991, AICHE Student Chapter Georgia Tech.
- 8. Outstanding Faculty Award, 1990-1991, Chemical Engineering, Georgia Tech.
- 9. Named Institute Fellow, 1994, Georgia Tech.
- 10. Research Program Development Award, 1995, Georgia Tech.

- 11. Research Award: NSF-ERC in Electronic Packaging, 1999.
- 12. Zeigler Outstanding Faculty, 2000-2001, School of Chemical Engineering, Georgia Tech.
- 13. Carl Wagner Memorial Award, The Electrochemical Society, 2001.
- 14. Named Fellow of The Electrochemical Society, October 2002.
- 15. Best Paper Award, IEEE 52<sup>nd</sup> Electronic Components and Technology Conference, 2002.
- 16. Thomas D. Callinan Award, Electrochemical Society, 2008.

# **SCHOLARLY ACCOMPLISHMENTS**

## A. Published Books and Parts of Books

- Hodge, T.C., Kohl, P.A., Bidstrup, S.A., Lee, J.B., and Allen M.A., "In-situ thermal Expansion Measurements of Interlevel Dielectric Polymer Films", Polyimides: Trends in Materials & Applications, (C. Feger, M. Khojasten, S. Molis Eds.) 287-302, Society of Plastic Engineers.
- Kohl, P. A., "Electrodeposition of Gold", in *Modern Electroplating*, (M. Schlesinger, M. Paniov, Eds) Wiley and Sons, 2000.
- Faulkner, L. R., Bullock, K. R., Kohl, P. A., Kukkonen, C. A., Maclachlan, A., McIntyre, J. A., Miller, B., Morrison, D. L., Vyas, B., and Weaver, R. D., "Effectiveness of the United States Advanced Battery Consortium as a government-Industry Partnership", National Research Council, 1998.
- Kohl, P. A., "Air-Gaps for Electrical Interconnections", in *Encyclopedia of Materials: Science and Technology* (H. L. Gossmann Ed), Pergamon, 2000.
- Kohl, P.A., Chapter 8: "Chip-to-Module Interconnection" in "Interconnect Technology and Design for Gigascale Integration", J. Davis, and J. D. Meindl, Ed., 2003.
- Meindl, J. D., Davis, J., Zarkesh-Ha, P., Patel, C., Martin, K. P., and Kohl, P.A., Chapter 1: "Interconnect Opportunities for GSI" in "Interconnect Technology and Design for Gigascale Integration", J. Davis, and J. D. Meindl, Ed., 2003.
- Kohl, P. A., Chapter on "Compliant Interconnects" in "New Trends in Electrochemical Technology", Eds: M. Datta, T. Osaka, and J. W. Schultze, 2004.
- Kohl, P. A., Osborn, T., and He, A., Chapter on "Advanced Chip-to-Substrate

Connections", in *Materials for Advanced Packaging*, Eds. Wong and Lu, Wiley, 2008.

Prakash, S., Mustain, W., and Kohl P. A., "Electrolytes for Long-Life, Ultra Low-Power Direct Methanol Fuel Cells" in *Advances in Fuel Cells*, Elsevier, 2008.

## B. Published Refereed Journal Papers

- Kohl, P.A., and Bard, A.J., "The Characterization and Behavior of n-Type ZnO, CdS and GaP Electrodes in Acetonitrile Solutions", <u>Journal of the American</u> <u>Chemical Society</u>, <u>99</u>, 7531-7539 (1977).
- 2. Kohl, P.A., Frank, S.N., and Bard, A.J., "Behavior of n- and p-Type single Crystal Semiconductors Covered with Thin n-Ti0<sub>2</sub> Films", <u>Journal of the Electrochemical Society</u>, <u>124</u>, 225-229 (1977).
- 3. Noufi, R.N., Kohl, P.A. and Bard, A.J., "Electrochemistry and Electroluminescence at n-Type TiO<sub>2</sub> in Aqueous Solutions", <u>Journal of the Electrochemical Society</u>, <u>125</u>, 246-252 (1978).
- 4. Noufi, R.N., Kohl, P.A. and Bard, A.J., "Photoelectrochemical Cells with Mixed Polycrystalline n-Type CdS-CdSe Electrodes", <u>Journal of the Electrochemical Society</u>, <u>125</u> 375-379 (1978).
- 5. Kohl, P.A. "The Electrochemical Behavior of n- and p-GaAs and InP in Nonaqueous Solutions", <u>Journal of the Electrochemical Society</u>, <u>125</u>, 283-286 (1978).
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- 7. Kohl, P.A., and Bard, A.J. "The Photoelectrochemical Behavior of n- and p-InP Electrodes in Acetonitrile Solutions", <u>Journal of the Electrochemical Society</u>, <u>126</u>, 598-602 (1979).
- 8. Kohl, P.A., and Bard, A.J., "Liquid Junction Photovoltaic Cells Based on n-GaAs Electrodes in Acetonitrile Solutions", <u>Journal of the Electrochemical Society</u>, <u>126</u>, 603-608 (1979).
- 9. Noufi, R.N., Kohl, P.A., Rogers, J.W., White, J.M., and Bard, A.J., "An Investigation of S/Se Substitution in single Crystal CdSe and CdS Photoelectrodes by Electron Spectroscopy", <u>Journal of the Electrochemical Society</u>, 126, 949-954 (1979).
- 10. Ostermayer, F.W. Jr. and Kohl, P.A., "Photoelectrochemical Etching of p-GaAs", Applied Physics Letters, 39, 76-78 (1981).

- 11. Kohl, P.A., "High Speed Solder Plating Baths", <u>Plating and Surface Finishing</u>, 45-48 (1981).
- 12. Kohl, P.A., Wolowodiuk, and Ostermayer, F.W., Jr., "The Photoelectrochemical Oxidation of (100), (111) and (111) n-InP and n-GaAs", <u>Journal of the Electrochemical Society</u>, <u>130</u>, 2288-2293 (1983).
- 13. Kohl, P.A., "The High Speed Electrodeposition of Sn/Pb Alloys", <u>Journal of the Electrochemical Society</u>, <u>129</u>, 1196-1199 (1982).
- 14. Kohl, P.A., "Hochgeschwindigkeitsabscheidung von Sinn-Blei-Legierungen". Oberflache Surface, 23 (b), 190-194 (1982).
- 15. Forrest, S.R., Kohl, P.A., Panock, R., DeWinter, J.W., Nahory, R.E., and Yanowski, E., "A Long-wavelength, Annular In<sub>0.53</sub>Ga<sub>0.47</sub>As, p-i-n Photodector", <u>IEEE Electron Device Letters</u>, <u>EDL-3</u>, 415-417 (1982).
- Ostermayer, F.W., Kohl, P.A., and Burton, R.H., "Photoelectrochemical Etching of Integral Lenses on InP/InGaAsP LEDs", <u>Applied Physics Letters</u>, <u>43</u>, 642-644 (1983).
- 17. Ostermayer, F.W., Kohl, P.A., and Lum, R.M., "Hole Transport Equation Analysis of Photoelectrochemical Etching Resolution", <u>Journal of Applied Physics</u>, <u>58</u>, 4390-4395 (1985).
- 18. Kohl, P.A., D'Asaro, L.A., Wolowodiuk, C. and Ostermayer, Jr., F.W., "Photoelectrochemical Plating of GaAs FETs", <u>Electron Device Letters</u>, <u>EDL-5</u>, 7-9 (1984).
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- 21. Lum, R.M., Ostermayer, F.W., Kohl, P.A., Glass, A.M., and Ballman, A.A., "Improvements in the Modulation Amplitude of Submicron Gratings Produced in n-InP by Direct Photoelectrochemical Etching", <u>Applied Physics Letters</u>, <u>47</u>, 269-271 (1985).
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- 36. Propst, E., Rieger, M., and Kohl, P.A., "Luminescence and its Quenching From Porous Silicon Formed in a Non-aqueous Electrolyte" <u>Applied Physics Letters</u>, <u>64</u>, 1914-16 (1994).

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- 49. Gray, G., Kohl, P.A., and Winnick, J., "Stability of Sodium Electrodeposited

- from a Room Temperature Chloroaluminate Molten Salt", <u>Journal of the Electrochemical Society</u>, <u>142</u>, 3636-3642 (1995).
- 50. Gray, G., and Winnick, J., and Kohl, P.A., "Plating and Stripping of Sodium from a Room Temperature 1,2-Dimethyl-3-propylimidazolium Chloride Melt", Journal of the Electrochemical Society, 143, 2262 (1996).
- 51. Rieger, M.M., Dudel, F.P., Pickering, J.P., Gole, J.L., Kohl, P.A., and Bottomley, L.A., "Photoluminescence in the Earliest Stages of Porous Silicon Formation", <u>Journal of The Electrochemical Society</u>, 143, L164 (1996).
- 52. Lee, J.B., Allen, M.A., Hodge, T.C., Bidstrup, S.A., and Kohl, P.A., "Modeling of Substrate-Induced Anisotropy in Through-Plane Behavior of Polymeric Thin Films", <u>Journal of Polymer Science</u>, Part B, Polymer Physics, <u>34</u>, 1591-1596, 1996.
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- 54. Gray, G.E., Winnick, J., and Kohl, P.A., "Plating and Stripping of Sodium from a Room Temperature 1-methyl-3-propylimidazolium Chloride Melt" <u>Journal of the Electrochemical Society</u>, <u>143</u>, 3820-24 (1996).
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- 56. Pye, S., Winnick, J., and Kohl, P.A., "Iron, Copper, and Nickel Behavior in Buffered, Neutral Aluminum Chloride: 1-Methyl-3-Ethylimidazolium Chloride Molten Salt", Journal of the Electrochemical Society, 144, 1933-8 (1997).
- 57. Hodge, T.C., Grove, N.R., Sinno, B., Bidstrup, S.A., and Kohl, P.A., "Stresses of Spin-Cast Polymer Films on Silicon Substrates", <u>Journal of Microcircuits and Electronic Packaging</u>, 20, 12-20 (1997).
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#### Patents Granted

- 1. Spray Cell for Selective Metal Deposition or Removal. R.R. Buckley and P.A. Kohl, Patent Number: 4,229,269.
- 2. Preventing Stains on Multiple Electroplated Articles. P.A. Kohl, Patent Number: 4,236,976.

- 3. Solder Plating Process. P.A. Kohl, Patent Number: 4,263,106.
- 4. Electrolytic Plating. P.A. Kohl, Patent Number: 4,310,392.
- 5. Photoelectrochemical Etching of Semiconductors. P.A. Kohl and F.W. Ostermayer, Patent Number: 4,369,099.
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- 1. Divisional Editor for the Electrochemical Society
- 2. Reviewer for:

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Science Foundation of Ireland

- 3. Publication Committee of the Journal of the Electrochemical Society
- 4. Editor (Founding Editor) of The Electrochemical Society Interface, 1992-1995.
- 5. Editor-in-Chief, Journal of The Electrochemical Society, 1995-present.
- 6. Editor-in-Chief (Founding Editor), Electrochemical and Solid-State Letters, 1998-2003.

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D. Please provide any available data or information on market potential/size.							
E. Is work on the invention continuing?   Yes No							
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# Fabrication of Microchannels using Polynorbornene Photosensitive Sacrificial Materials

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#### ABSTRACT

A processing method has been demonstrated for the fabrication of microchannels by using photosensitive polynorbomene copolymer based sacrificial materials. The channel geometric patterns of sacrificial polymer were made via photolithography. The sacrificial polymer patterns were encapsulated with a dielectric medium and then thermally decomposed to form air channels. For the thermal decomposition of sacrificial polymer, the heating program was determined on the basis of the kinetic model obtained from TGA analysis to maintain the decomposition at a constant rate. The results indicate that a properly selected heating program can avoid the deformation in the channel structure; at the same conditions, a large-size channel is more easily to be deformed than a small one. The tapered-structure microchannels were also produced using a gray-scale mask. The result shows that a suitably low contrast for the photosensitive sacrificial material can lead to smooth and tapered microchannels.

Keywords: microchannel, polynorbornene, photolithography, thermal decomposition, contrast

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#### INTRODUCTION

Microfluidic devices have tremendous potential for applications in a variety of fields including drug discovery, biomedical testing, and chemical synthesis and analysis. In such devices, liquids and gases are manipulated in microchannels with cross-sectional dimensions on the order of tens to hundreds of microns. Processing in such microchannel devices offers a number of advantages including low reagent and analyte consumption, highly compact and portable systems, fast processing times, and the potential for disposable systems. However, in spite of all of their promise, microfluidic devices are currently being used in a limited number of applications and are in general still rather simple devices in terms of their operational complexity and capabilities. For example, in terms of making truly portable microanalytical systems, one of the current difficulties involves the simple integration of electronic (e.g. sensing methods) and fluidic elements into the same device. One of the most important issues, which controls this ability to integrate functions into the same device and thus controls the level of functionality of a microfluidic device is the method used to fabricate the structure.

The two most prevalent methods for fabricating microfluidic devices to date involve either bonding together layers of ultraflat glass or elastomeric polymers such as poly(dimethylsiloxane).<sup>4</sup> Both methods suffer from severe limitations and difficulties associated with integrating non-fluidic elements such as detectors with the microchannel system in the same substrate.<sup>4-6</sup> A method developed recently, which uses microchannel fabrication methods that are completely compatible with standard silicon CMOS processes, can overcome many of these limitations and thus permit the integration of

electronic control, actuation, and detection systems into a single device during the same fabrication sequence.<sup>7</sup> The first version of this method involves the use of a sacrificial polymer (polynorbornene) as a structural place-holder for channel formation using a conventional semiconductor process flow. The sacrificial polymer is first deposited as a blanket film by spin-casting or other deposition methods. A protective etch hard mask such as silicon dioxide is then coated onto the polymer layer and patterned using conventional photolithography and oxygen plasma etching. This patterned hard mask protects the underlying polymer from the etchant, leaving behind polymer relief patterns. These polymer structures are overcoated with a permanent structural material such as a polyimide or oxide. This sequence can be repeated to build up multilayer channel structures. Once all of the desired structures are formed, the entire device is heated to the decomposition temperature of the sacrificial polymer, leaving behind open microchannel structures.

This first sacrificial polymer fabrication method suffers from several limitations including the fact that it requires on the order of ten processing steps to complete the sequence for a single level of microchannels. Recently, an improved sacrificial polymer method using photodefinable norbornene copolymers was reported which completely eliminates the need for hard mask deposition, photoresist patterning, and plasma etching. This improved method thus dramatically reduces the number of process steps required, resulting in a process that can be completed in only five steps (see Figure 1).<sup>8, 9</sup> In addition to significantly reducing the number of process steps required, this new method also opens up the possibility of forming arbitrarily shaped, three dimensional channel structures using gray scale lithography as suggested in our prior publication.<sup>9</sup>

These photosensitive norbornene copolymer sacrificial materials consist of formulations of copolymers of pendant butyl- and alkenyl-substituted norbornenes (PNB) with small additions of a photoinitiator (PI) to selectively induce crosslinking. The photolithographic characteristics, photoinitiation systems, and thermal decomposition properties of these sacrificial materials has been systematically investigated in previous studies. These experimental results provide the basic information required for the fabrication of microchannels using these sacrificial materials. However, it was shown in the work of Bhusrai, et al. that the cross sectional shape of channel structures produced using these sacrificial polymer methods may be arched under certain processing conditions. This unintentional curvature was ascribed to possible flow of the overcoat medium during the relatively high temperature decomposition process. However, no further information was available at the time however that could be used to guide process design to prevent this deformation in channel shape. The ability to prevent channel deformation is particularly important when the goal of the fabrication sequence is to build channels with controlled three dimensional cross sectional shapes.

The main goal of this work is to further develop and demonstrate the use of photodefinable sacrificial polymer fabrication methods to produce channel geometries with arbitrarily shaped cross-sectional profiles. This ability to control the shape of the channel cross-section is expected to be particularly useful in precisely controlling the flow of fluids in microchannel systems. The ability to control fluid flow patterns and dispersion by controlling the channel cross section is investigated in this work through computational fluid dynamics simulations. It was found that tapered cross sectional channel profiles are useful in preserving "plug flow" conditions in curved microchannels

and thus reducing dispersion of components in the flow. Therefore, the thermal decomposition of the photodefinable sacrificial polymers was studied in detail and novel heating protocols were developed that maintain the channel shape during decomposition. The use of these methods is finally demonstrated using grey scale lithography to produce microchannels with tapered cross sections.

#### SIMULATION OF FLOW IN CURVED CHANNELS

When designing and fabricating microfluidic devices, it is almost inevitable that channels with curved shapes will be required. For example, when designing a long separation column on a chip, turning the channel into a meandering path may be required to keep the device within some required size limits. In such cases, it can be extremely important to precisely control the fluid flow pattern in the channel so as to minimize differences in the residence time distribution of fluid traveling through the channel. In other words, one generally would like to maintain near "plug flow" conditions in devices used for separations, analysis, and other fluidic operations to prevent mixing and loss of spatial confinement of fluid samples after injection or separation. One particular problem is minimizing residence time variations for fluids traveling through corners and curved sections of microfluidic channels. In order to illustrate this point and investigate the improvements that could be realized by using channels with tapered cross sections, a series of computational fluid dynamics simulations were performed.

Fluent, a computational fluid dynamics (CFD) simulation package produced by Fluent Inc., was used to simulate the flow in a series of different corner designs for microchannels. GAMBIT, a preprocessor accessory for FLUENT made by Fluent Inc.,

was used to construct the desired model geometry, apply the meshing points to the model, and define the required boundary zones. Once defined, Fluent was used to simulate the flow pattern in each microchannel and to produce numerical and graphical results for each case.

In this work, a series of 90 degree turns in microchannels were simulated with varying cross sectional geometries. Figure 2 shows the cross sections of the four simulated channels. Fig. 2a shows the dimensions of a uniform area channel. Figures 2 b and 2c show channels with tapered corners. The taper improved the flow around corners with 2c representing a near optimized design. The inside radius of the turns was held constant at 60 µm and the outside radius of the turns was held constant at 120 µm. The same boundary conditions were applied in simulating the flow through these channels and a constant pressure outlet condition which was assumed to be atmospheric pressure. In this case, water was used as the flow media, but the results should be general to any Newtonian fluid under laminar flow conditions. Under these conditions, the flow rates and Reynolds numbers are quite low which indicates laminar flow conditions, and thus a laminar flow model was used in Fluent for solution of these problems. In order to look at the dispersion which would occur in fluid flowing around each of these microchannel corners, fluid packet trajectories and transit times around each turn were calculated. Figure 3 shows plots of the transit times for fluid packets as a function of radial distance along the corner for each type of turn structure. The appearance of different lines of packet transit times on these plots are due to the fact that fluid packets at different vertical positions within the channels also experience slight dispersion due to low velocities near the top and bottom surfaces of the channel.

Figure 3A clearly shows that the standard rectangular channel geometry would result in severe dispersion of an initially flat concentration profile after traveling around the 90 degree turn. Under laminar flow conditions, the relatively uniform velocity profile across the channel cross section coupled with the longer path length for fluid at the outside of the turn result in transit times which are a factor of 3 to 5 larger for fluid at the outside radius as compared to fluid at the inside radius. This dispersion would be even more greatly exaggerated for the case of a 180 degree bend. One natural solution to this problem is to decrease the velocity of the fluid near the inside radius of the turn in order to achieve equal transit times for the fluid irrespective of radial position. One way to achieve this velocity modification is to alter the cross sectional area of different regions of the channel. Figure 3B shows the transit time profile for fluid flowing around a turn in a triangular cross section channel. The reduced channel height at the inside radius of the turn would be expected to slow the velocity of fluid along the inside of the turn. Indeed, Figure 3B shows that the triangular cross section overcompensates and results in longer transit times for fluid near the inside radius as compared to fluid near the outside radius. From close inspection of the Fluent results, it is also apparent that channel sections which have two walls intersecting at acute angles leads to significant dispersion in these regions, and thus acute angles in the channel cross section geometry should be avoided if possible. Based on these facts, a series of rough optimizations were performed to design an improved channel cross section profile that would result in minimal dispersion around the simulated turn. Figure 3C shows the fluid transit time results for such an improved channel structure. The transit time profile is essentially uniform for fluid flowing around a 90 degree corner using this improved shape. Thus, it is clear that by engineering the cross-sectional shape of microchannels in turns it should be possible to minimize dispersion in the flow profiles.

#### **EXPERIMENTAL**

The sacrificial polymer used in this work, which consists of the copolymer of butyl norbornene (BuNB) and alkenyl norbornene (ANB) in the molar ratio 73/27, was synthesized and supplied by Promerus LLC (Brecksville, OH). The polymer weight average molecular weight (M<sub>w</sub>) and polydispersity index (PDI) were measured to be 425,000 and 3.74 respectively by gel permeation chromatography using polystyrene calibration standards. Bis(2,4,6-trimethylbenzoyl)-phenylphosphineoxide (Irgacure 819, Ciba Specialty Chemicals Inc.) was used as a PI for this work. Solutions of polynorbornene (PNB) and PI were prepared using mesitylene (MS, 97%, Aldrich) as the solvent. Two different formulations, PNB/PI/MS in a mole ratio of 16/0.32/84 (2 wt% initiator relative to dry polymer) and PNB/PI/MS in a mole ratio of 16/0.64/84 (4 wt% initiator relative to dry polymer) (weight ratios), were used in the experiments. After exposure and baking, polymer patterns were developed using xylene (98.5+%, Aldrich).

Thermal decomposition characteristics of the sacrificial polymer were investigated using a Seiko Instruments Inc. TG/DTA 320 system. Thermogravimetric analysis (TGA) measurements were performed under N<sub>2</sub> at a purge rate of 28 ml/min. The encapsulated sacrificial polymer structures were thermally decomposed in a Lindberg tube furnace purged with N<sub>2</sub>.

For microchannel fabrication, PNB/PI films were cast onto silicon wafers using a Brewer Science CEE 100 spinner and hotplate system. A 3.5 ~ 4.0 µm thick PNB/PI film

was obtained at a spin speed of 2400 rpm and a softbake of 110°C for 60 seconds. Film thicknesses were measured using a Veeco Dektak profilometer. An OAI Mask Aligner equipped with an *i*-line filtered UV irradiation source (365 nm wavelength) was used to expose and pattern the PNB/PI films. Before exposure, the intensity of UV light source was measured using an OAI Model 356 Exposure Analyzer with a 365 nm probe. After exposure, samples were post-exposure baked at 120°C for 30 minutes in an oven. Samples were developed using a continuous spray of xylene while the wafer was spun at 500 rpm.

Removal of any polymer residue from the developed patterns was accomplished using a PlasmaTherm reactive ion etching (RIE) system using the following conditions: 5 sccm CHF<sub>3</sub>, 45 sccm O<sub>2</sub>, 250 mTorr, 300 W, 35°C. The etching rate of the polymer under these conditions is approximately 300 nm/min. Plasma enhanced chemical vapor deposition (PECVD) was performed to deposit an SiO<sub>2</sub> overcoat for encapsulation of the polymer channel patterns. The SiO<sub>2</sub> was deposited with a PlasmaTherm PECVD using the following conditions: 380 kHz RF frequency, 50W power, 200°C, 550mTorr, and a gas mixture of N<sub>2</sub>O (1400 sccm) and 2% SiH<sub>4</sub> diluted in N<sub>2</sub> (400 sccm). The deposition rate for the oxide using these conditions is approximately 50 nm/min.

### **Thermal Decomposition Program**

For the thermal decomposition process, the fractional decomposition can be calculated from the TG curve as shown in equation (1):

$$\alpha = \frac{W_0 - W}{W_0 - W_f} \tag{1}$$

where  $W_0$  is the initial mass, W is the mass remaining at some time during the decomposition, and  $W_f$  is the final mass of the sample at the end of the thermal cycle. The kinetic description for thermal decomposition of the polymer is generally expressed as shown in equation equation (2):

$$\frac{d\alpha}{dt} = k(1-\alpha)^n = A \exp(-\frac{E_u}{RT})(1-\alpha)^n$$
 (2)

where n is the overall order of decomposition reaction, A is the Arrhenius pre-exponential factor, and  $E_a$  is the activation energy of the decomposition reaction.

In order to avoid a sudden and large release of the gaseous decomposition products from the polymer patterns that may result in distortion of the channel structure, it is desired to keep the decomposition rate  $\left(\frac{d\alpha}{dt}\right)$  constant during the entire decomposition process. Assuming the decomposition rate is equal to a constant, r, throughout the decomposition process then:

$$\frac{d\alpha}{dt} = r \text{, and, } t = 0, \ \alpha = 0 \tag{3}$$

Integrating equation (3) gives the general desired result shown in equation (4):

$$\alpha = rt$$
 (4)

Assuming that the reaction order, activation energy, and pre-exponentional factor do not change significantly during the decomposition,  $\frac{d\alpha}{dt}$  and  $\alpha$  can be replaced with r and rt respectively in equation (2) which results in the following equation:

$$r = A \exp(-\frac{E_u}{RT})(1-rt)^n \tag{5}$$

It is now possible to rearrange equation (5) to solve for the necessary temperature versus time profile that is required to maintain a constant rate of polymer decomposition throughout the entire process. The explicit expression for temperature versus time is shown in equation (6).

$$T = \frac{E_u}{R} \left[ \ln \frac{A(1 - rt)^n}{r} \right]^{-1}$$
 (6)

Thus, in order to design a heating profile it is necessary to specify only four parameters: the three kinetic parameters  $(A, E_a \text{ and } n)$  that describe the polymer decomposition, and r the desired polymer decomposition rate. Based on regression of TGA data performed in previous experiments<sup>9</sup>, the kinetic parameters for the polymer used in this work were determined to be:  $A = 5.835 \times 10^{14} \text{ min}^{-1}$ ,  $E_a = 207 \text{ kJ/mol}$  and n = 1.05. Thus, for a given constant decomposition rate, r, one can obtain a curve of temperature versus decomposition time.

### RESULTS AND DISCUSSIONS

Decomposition Condition: Thermal decomposition of the sacrificial polymer was performed in a pure nitrogen atmosphere in order to avoid any oxidation of the polymer that could result in the formation of non-volatile decomposition products and undesirable residue in the microchannels. In addition to using an inert atmosphere, as suggested previously a controlled heating profile was used to maintain a relatively constant polymer decomposition rate. This constant decomposition rate ensures that gaseous products are not released so quickly that pressures high enough to significantly deform the channel shape are generated.

Figure 4 shows curves of the decomposition rate versus time for pure PNB samples decomposed at both a constant temperature of 425°C (isothermal decomposition) and various heating rates (dynamic decomposition) respectively. In each case, there is a peak in the decomposition rate. The width of the peak corresponds to the transition period during the conversion of sacrificial polymer to gaseous products. Higher heating rates or high temperature isothermal decompositions result in a sharp peak in the decomposition rate profile. This implies that the majority of the decomposition process occurs over a short time interval, thus resulting in a sudden and large release of the gaseous decomposition products. It was therefore expected that controlling the decomposition rate at a constant low level using controlled heating profiles could eliminate this phenomena and thus prevent channel distortion during decomposition. It was decided to test this theory by comparing the effect of various decomposition procedures on the final resulting microchannel shapes and sizes.

Based on equation (6), the temperature versus time heating profiles required to achieve decomposition rates of 1, 2 and 3 %/minute were calculated and are shown in Figure 5. The figure illustrates that, at a constant decomposition rate, the decomposition temperature during most of decomposition time should be set relatively low with a slight ramp rate. However as the decomposition nears completion, higher temperatures can be used which helps obtain complete decomposition of the polymer within a reasonable time scale.

In order to preclude the need for complex temperature controllers for the decomposition furnaces used in the microchannel fabrication process, representative temperature profiles that closely approximate the smooth temperature versus time curves

produced using equation (6) were used. Figure 6 shows the temperature versus time curve calculated using equation (6) and the corresponding simple mimic heating profile that was tested in the Lindberg decomposition furnaces for device fabrication. Figure 7 shows TGA results for the simple mimic heating program that was designed to achieve a 1%/minute decomposition rate. The DTG curve demonstrates that the decomposition rate does indeed fluctuate closely around the desired 1%/minute level without extreme variations. Thus, the sharp peak in the decomposition rate shown in Figure 4 can be avoided by using more intelligent heating profiles. When this same mimic heating profile is used in processing encapsulated polymer samples, no distortion in the encapsulated channels was observed but electron microscopy revealed that small amounts of polymer residue were left in the channel structures. Two different modifications to the mimic heating profile were tested in an attempt to remove this residual polymer. In the first case, a final hold at 455°C for one hour was used in an attempt to remove the residual polymer. This high temperature hold did indeed reduce the residual remaining polymer substantially as observed in SEM cross sections, but some remaining residue was left even after the one hour hold. A second method which involved doubling the intermediate holds shown in Figure 6 was also tested. This effectively reduced the average decomposition rate even further to somewhere approaching the 0.5%/minute level. In this case, it was observed that no distortion of the channel profile occurred during the decomposition and essentially no polymer residue was found in the microchannel after decomposition. This suggests that there may be additional byproducts formed during the decomposition if the process is ramped too quickly which result in a residue that can be difficult to remove with even high temperature processing. Longer holds at lower temperatures can be used to both slow the decomposition rate and thus reduce pattern profile distortion and to eliminate residual polymer in the final channel structures.

Microchannels encapsulated with polyimide and SiO<sub>2</sub>: Microchannels have been made following the scheme in Figure 1. In the processing, a 3.5 ~ 4.0 µm thick PNB/PI film (4 wt% initiator in PNB) was cast using a spin speed of 2400 rpm and softbake condition of 110°C/60 seconds. The film was exposed to UV light using a chrome on quartz mask with dose of 450 mJ/cm<sup>2</sup> and post-exposure baked at 120°C for 30 minutes in an oven. After post-exposure baking, the film was spray developed using xylene to produce the desired channel patterns. There was no noticeable residue remaining after development in the patterned areas, but direct overcoating of the encapsulant material on the asdeveloped features resulted in poor adhesion to the substrate. In fact, small bubbles were observed to form in the overcoat materials in the areas where the sacrificial polymer was presumably developed cleanly away from the substrate. Therefore, it was concluded that there must be some small amount of remaining polymer residue after development that prevents good adhesion of the overcoat to the substrate. In order to avoid this phenomenon, a residue removal treatment was employed by dry etching in an oxygen plasma using an RIE before the channel patterns are encapsulated. After residue removal using the plasma, samples were then encapsulated using either polyimide or SiO<sub>2</sub>. Polyimides are good materials for encapsulation because they display high glass transition temperatures and thermal stability, low dielectric constant, modulus, moisture adsorption and stress<sup>7</sup>. In this work, HD Microsystems PI 2734 polyimide, was used to overcoat some of the channel structures. In these cases, the PI 2734 was spin-coated on the top of the channel patterns at a speed of 2300 rpm for 30 sec, and cured at 350°C for 1 hr under  $N_2$ . The thickness of the polyimide layer under these conditions is approximately 4.5  $\mu$ m. In addition, some channel structures were encapsulated using SiO<sub>2</sub>. In these cases, a 2  $\mu$ m thick encapsulation layer of SiO<sub>2</sub> was deposited using the PECVD recipe described earlier.

The decomposition of the encapsulated polymer patterns was performed at various decomposition rates to investigate the effect of the rate on the channel structure. Figures 8a through 8g show SEM images of the channel encapsulated with polyimide and decomposed at different rates using different heating profiles. The results indicate that the decomposition rate does indeed affect the channel structure significantly. At low decomposition rates (1 or 2%/minute), the channel structures produced maintain the size and shape of the original PNB sacrificial polymer pattern. However, at relatively high decomposition rates (3%/min) or when a high constant temperature decomposition process is used, the microchannels are distorted into dome or arc shaped profiles. It is also obvious that this distortion problem becomes a more important issue for microchannels as their lateral size increases. Channels with larger widths clearly SEM images of channels deformed more than channels of smaller dimensions. encapsulated with SiO<sub>2</sub> are shown in Figures 9a to 9f. It was observed that the extent of channel deformation appears to be higher in the SiO<sub>2</sub> overcoated structures as compared to the polyimide overcoated channels at the same nominal channel feature sizes and polymer decomposition rates. This larger deformation in the SiO<sub>2</sub> overcoated samples could be due to both differences in the mechanical properties of the two overcoat

materials and differences in the diffusion rate of the decomposition products through the overcoat materials.

Microchannels with tapered cross-section structure: As discussed previously, one of the goals of this work was to provide a simple fabrication method for microchannels with tapered cross sectional profiles that could be used to control fluid flow patterns in microchannels. In order to fabricate the tapered microchannel structures, the concept described here is to use a gray-scale lithography process employing a gray-scale photomask and a low contrast photosensitive sacrificial material. A series of experiments were performed to investigate the possibility of using such an approach for producing microchannels that are shaped in a controlled manner in all three dimensions.

On the mask used in these experiments, channel features were designed with an approximately linear gradient in percent transmission, which were made by patterning various regions or "zones" across the width of the channel with varying ratios of chrome stripes to clear transparent area. In this particular case, the chrome stripe features were designed to be 200 nm in size and thus served as sub-resolution features for the photosensitive sacrificial polymers used in this work. The masks were fabricated from these designs by electron beam lithography at ETEC Systems (Hayward, CA). Table 1 describes the two main channel features used in this work in more detail. Using this type of gray-scale mask allows for the photosensitive sacrificial material to be exposed to a range of doses across the width of the channel feature using a single lithographic exposure step. This exposure gradient in conjunction with a low contrast resist material can be used to produce a feature that is shaped in both the lateral and vertical directions

with respect to the plane of the substrate in a single lithographic process. Two photosensitive materials with different contrast levels were used to generate tapered microchannel structures with this mask. Figure 10 shows the contrast curves for the two photosensitive sacrificial polymer formulations used in this work. The methods of measuring contrast curves and calculating contrast values for these materials have been discussed previously in the literature.<sup>8,9</sup> The contrast factors for these two systems are a modest 0.51 and 0.85 for the 2wt% (referred to as material 1) and 4wt% (referred to as material 2) photoinitiator relative to dry polymer loadings respectively.

Using this contrast curve data, it is possible to quickly calculate a rough prediction of the pattern profile that will result from exposure using a gray-scale mask with these photosensitive materials if the relative transparency as a function of position on the mask is known accurately. Based on polynomial fitting, the contrast curves can be adequately described using the following functions:

$$f_l = 0.0236[log(D)]^3 - 0.357[log(D)]^2 + 1.8185[log(D)] - 2.127$$
 (7)

$$f_2 = 0.0352[log(D)]^3 - 0.6526[log(D)]^2 + 2.9467[log(D)] - 2.921$$
 (8)

Here  $f_i$  is the fraction of the film thickness remaining after exposure to a dose D and wet development for material i.

An approximate shape of the channel patterns that will be produced from a grayscale mask can thus be predicted using Eq. 9.,

$$d(x) = f_i(\log[D \cdot TP(x)]) \cdot FT, \tag{9}$$

where,  $f_i$  is the contrast function for material i, d(x) is the thickness of the film (after development) at a certain position x across the channel pattern, TP(x) is the fractional transparency of the mask at the position x across the feature, D is the nominal exposure dose used, and FT is the original thickness of the cast film. The outline of the simulated channel pattern consists of the points calculated by Eq. 9, which were then smoothed by seven-point smoothing, Eq. 10.

$$S_{i} = \frac{Y_{i-3} + 2Y_{i-2} + 3Y_{i-1} + 4Y_{i} + 3Y_{i+1} + 2Y_{i+2} + Y_{i+3}}{16}$$
 (10)

where  $S_i$  and  $Y_i$  are the smoothed signal and original signal for the  $i^{th}$  point respectively.

Tapered-structure channel patterns were fabricated using the gray-scale lithographic approach using a sequence of steps similar to those outlined in Figure 1. First, 12 μm thick PNB/PI films were cast using a spin speed of 700 rpm and softbake condition of 110°C for 2 minutes. The films were then exposed to UV light with the gray-scale mask. The nominal exposure dose was set using the contrast curve data for the photosensitive material to obtain a film with 80% original thickness remaining after development under a 100% transparent feature. The doses used were 1300 mJ/cm² and 165mJ/cm² for 2 wt% and 4 wt% initiator loadings respectively. The films were post-exposure baked at 120°C for 30 minutes in oven. The films were spray developed using xylene at a spin speed of 500rpm for 30 seconds. The final shape of the microchannel patterns was measured using profilometry.

Figures 11 and 12 show the real Feature I type PNB patterns produced as measured by profilometry, and for comparison the predicted microchannel patterns (using equations 7 through 10), for the systems with 2 wt% and 4 wt% initiator loadings. A comparison between different patterns produced by the two photosensitive materials clearly shows that the material with the lower contrast produces a profile that more closely resembles the desired smoothly tapered structure. However, it can be seen that the simple prediction of the profile shape only roughly approximates the actual feature produced using this method. Upon closer inspection of the mask, it was apparent that the desired smooth gradient in transmission was not faithfully reproduced into the mask due to the extremely small feature sizes used for the constituent patterns. This brings up the issue that accurate gray scale mask production for such a method may in fact be a challenging task. In any case, with more careful attention and accurate transfer of the design to the mask, it should be possible to use the contrast data for a material in conjunction with equations (7) through (10) to design a gray-scale mask feature for a specific photosensitive material that can be used in principle to obtain any desired pattern shape.

The tapered polymer microchannel patterns were next overcoated and decomposed in order to test the ability to transfer the tapered profile into the final microchannel. First, any polymer residue was removed from the substrate using an oxygen RIE plasma etch. The channel patterns were then encapsulated with SiO<sub>2</sub> using the same conditions described previously. The thermal decomposition of encapsulated channel patterns was performed under N<sub>2</sub> with a decomposition rate of 0.5%/minute. SEM images of the resulting tapered microchannels are shown in Figures 13a to 13d.

Due to the ability to carefully control the decomposition rate of the polymer by controlling the heating profile during decomposition, no deformation was observed in the channel structure. This can be seen by comparing the profiles of the original PNB patterns in Figures 11 and 12 with the SEM channel cross sections in Figure 13. The widths of the channels in Figure 13c and 13d are narrower than the feature sizes on the gray-scale mask due in part to slight RIE over-etching during the polymer residue removal step. Comparing figures 13a and 13b with figures 13c and 13d, it can be seen that a low contrast sacrificial material is desirable for the fabrication of smoothly tapered microchannel structures. As expected, the final shape of the channel structure is determined by a combination of the gray-scale pattern on the mask, the contrast of the photosensitive material, and the nominal exposure dose used in printing the feature.

In order to obtain an idea of the effectiveness of fabricated channel cross sections in reducing dispersion in flow around microchannel corners, the expected fluid transit times around a corner of the shape shown in Figure 11a were simulated using Fluent as described previously. Figure 14 shows the predicted transit times for flow around this corner using the boundary conditions and velocities used in the earlier idealized channel simulations. It is clear from this simulation that even the crudely shaped channel fabricated for demonstration purposes in this work would be expected to perform better than the standard rectangular cross section channel. Further, it is hoped that by optimizing mask design and process conditions, that a more ideal shape similar to that shown in Figure 3C can be achieved and used for device fabrication. This further refinement of the process is the subject of ongoing work.

### CONCLUSIONS

The fabrication of microchannels has been demonstrated by using photosensitive sacrificial polymer materials. The process consists of patterning the sacrificial polymer via photolithography, removal of polymer residue using RIE, encapsulation with a dielectric medium, and thermal decomposition of encapsulated polymer channel patterns. A method for designing heating programs to keep the thermal decomposition of sacrificial polymer at a constant rate was presented using the kinetic model of polymer decomposition. Heating programs designed using this approach have been demonstrated to prevent sudden and large decomposition rates (i.e. which result in drastic release of gaseous decomposition products that distort channel features), and were also shown to produce microchannel patterns with well controlled shapes that do not exhibit any substantial deformation after the thermal decomposition of the sacrificial polymer. Controlling the decomposition rate and slowly releasing the gaseous decomposition products allows the decomposition products to permeate through the overcoat at a rate roughly equivalent to the decomposition rate, and thus avoids the build-up of large pressures in the microchannel which can lead to distortion and failure of the structure. It was also found that larger channels have a higher tendency toward distortion. A grayscale lithographic process has been developed and demonstrated for the production of microchannels with tapered cross-sections. Such tapered channels have been shown through simulation to be able to reduce effects such as dispersion that are detrimental to microfluidic system performance.

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## Figure Captions

Figure 1. Schematic of processing steps for microchannel fabrication using photodefinable polymer sacrificial materials.

Figure 2. Schematic of microchannel cross sections simulated using Fluent.

Figure 3. Fluid transit time plots for flow around 90 degree turns with 60 micron inside radii for microchannel cross sections shown in Figure 2, (a) corresponds to Fig. 2a, (b) corresponds to Fig. 2b, and (c) corresponds to Fig. 2c.

Figure 4. Differential thermal gravimetric (DTG) curves for pure PNB samples decomposed at a constant temperature of 425°C (isothermal decomposition) or various heating rates (dynamic decomposition).

Figure 5. Calculated trends of temperature versus time for the decomposition of pure polymer at rates of 1, 2 and 3%/min.

Figure 6. Calculated and mimic heating programs for the decomposition of pure polymer at a rate of 1%/min.

Figure 7. TGA results for the mimic heating program set for a nominal decomposition rate of 1%/minute.

Figure 8. SEM images of the channels encapsulated with polyimide and decomposed with at rates of (a, b) 1%/minute, (c, d) 2%/minute, (e, f) 3%/minute, and (g) at a constant temperature of 425°C.

Figure 9. Microchannels encapsulated with SiO<sub>2</sub> and decomposed at rates of (a, b) 0.5, (c, d) 1, and (e, f) 3%/minute.

Figure 10. Contrast curves for photosensitive PNB formulations with various photoinitiator loadings: 2 and 4 wt% (in PNB).

Figure 11. Real and simulated channel patterns (with Feature I of the mask) for the system with 2 wt % initiator loading.

Figure 12. Real and simulated channel patterns (with Feature I of the mask) for the system with 4 wt % initiator loading.

Figure 13. SEM images of tapered microchannels made by using (a) Feature I of the gray scale mask with 2% PI, (b) Feature II with 2%PI, (c) Feature I with 4% PI, and (d) Feature II with 4% PI.

Figure 14. Fluent simulation of fluid transit times around 90 degree corner with 60 micron inside radius for microchannel with cross section similar to that shown in Figure 11a.

Table 1 Characteristics of the gray-scale microchannel photomask

Feature I

Channel Width

 $60 \, \mu m$ 

Zone Size:

6 µm 6 µm 6 µm 6 µm 6 µm

Transparency (TP):

100% 90% 80% ...... 30% 20% 10%

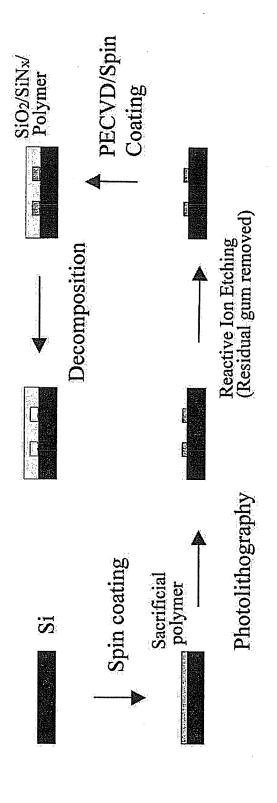
Feature II

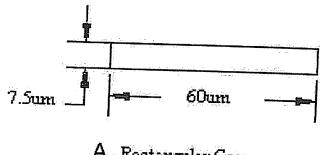
Channel Width

80 µm

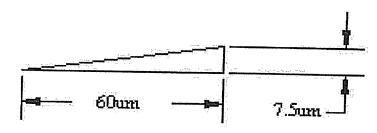
Zone Size:

Transparency (TP):

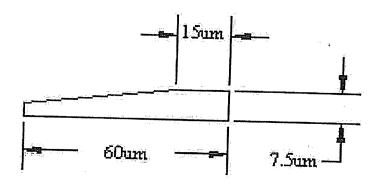




A. Rectangular Corner

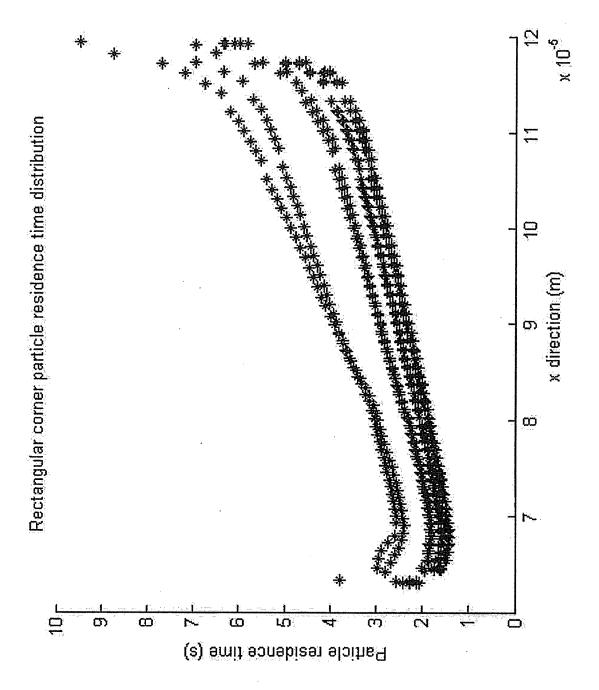


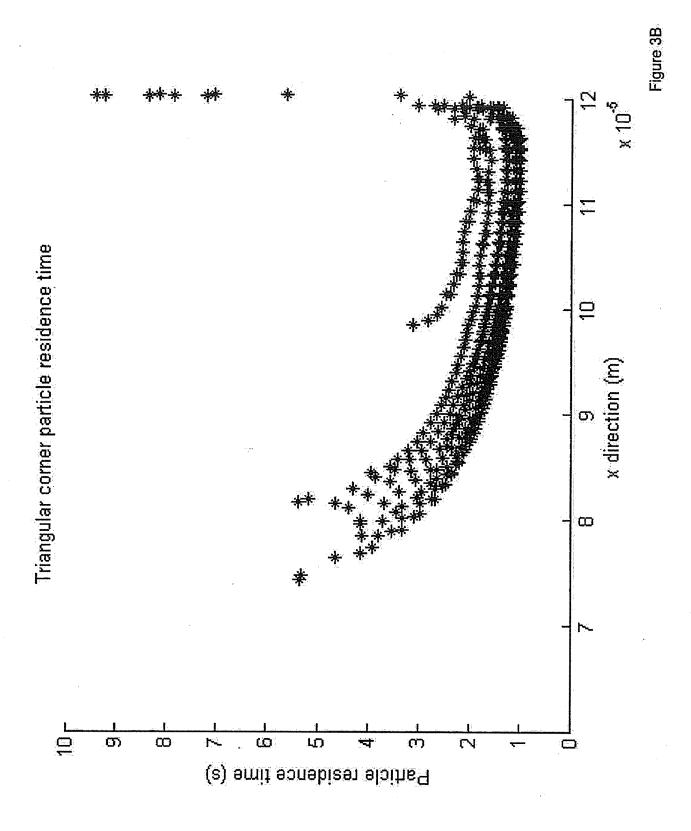
B. Triangular Corner

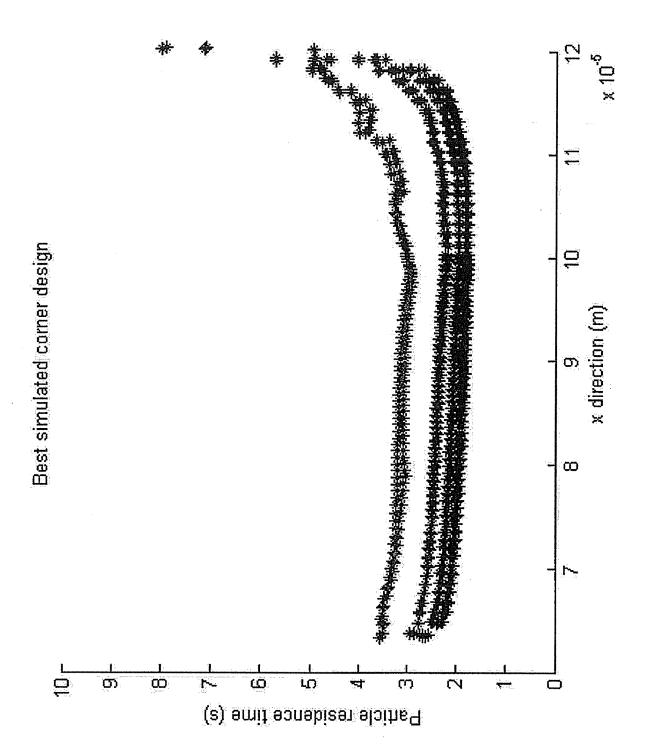


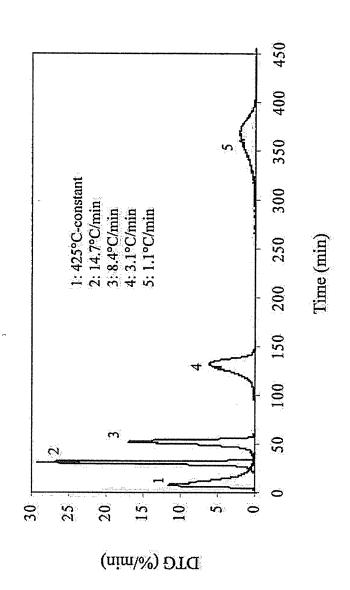
C. Best Simulated Corner

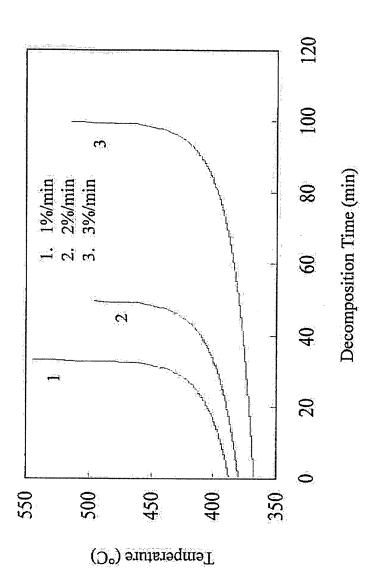
Figure 2

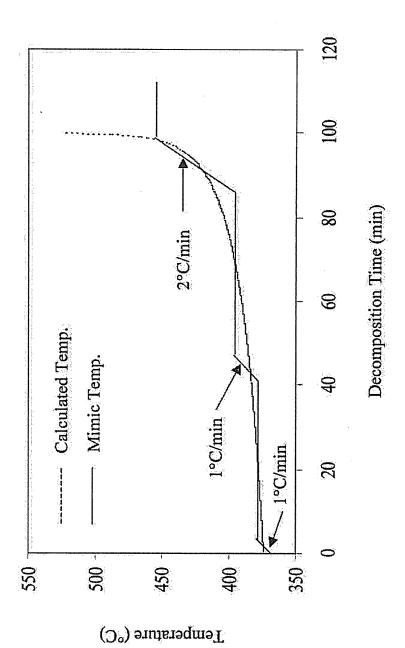




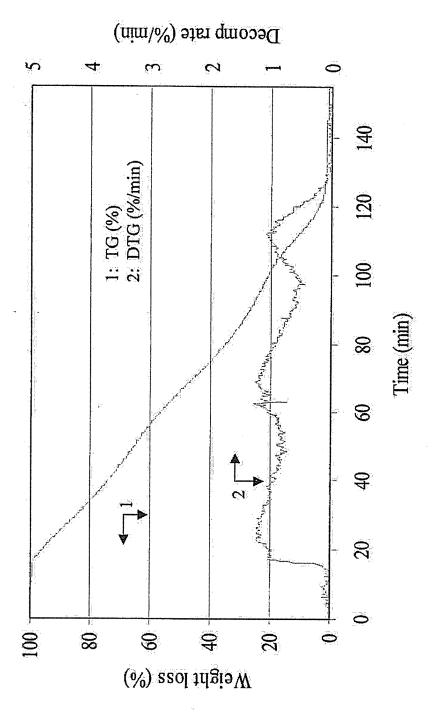


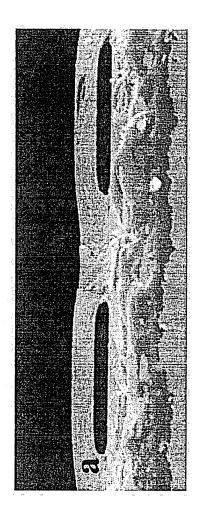


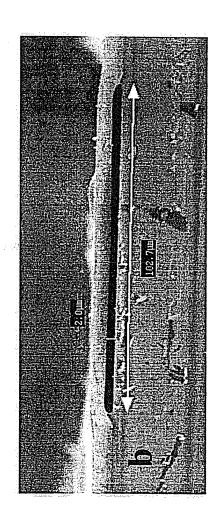


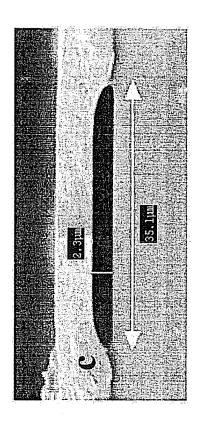


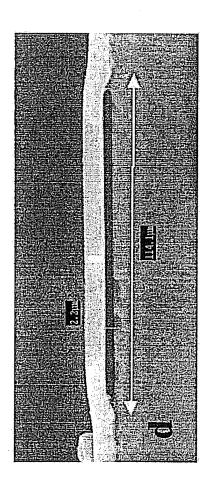


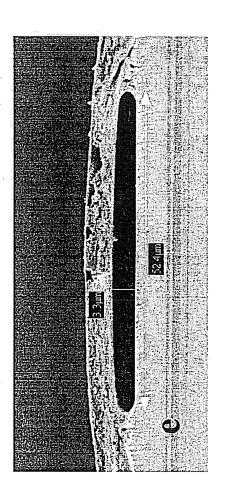


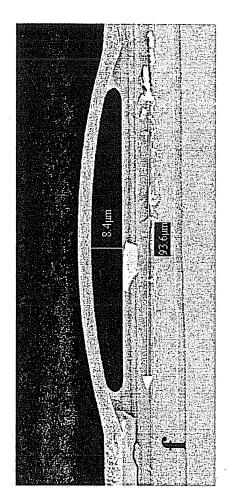


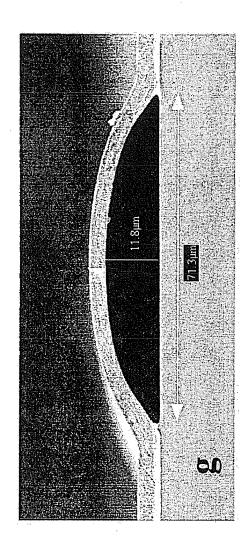


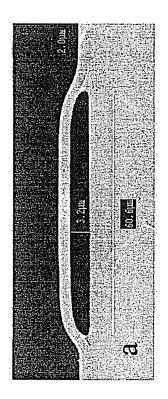


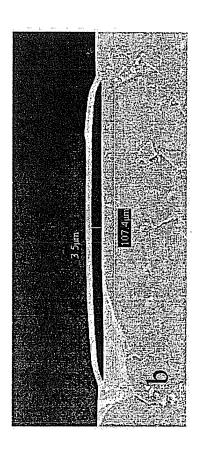


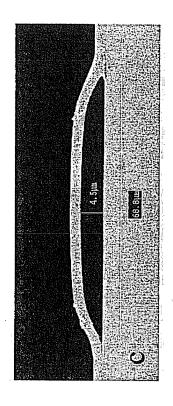


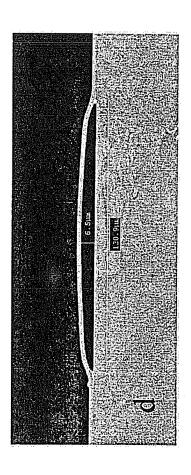


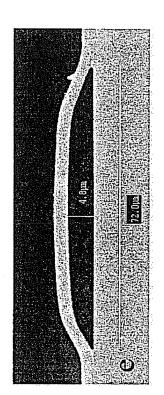


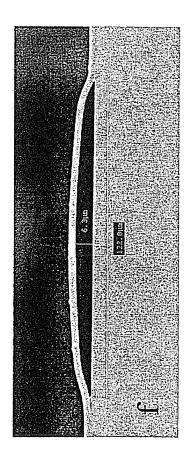


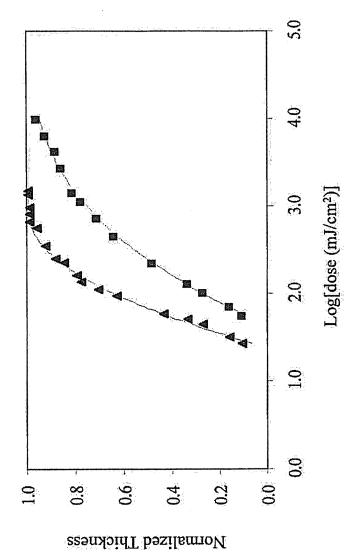












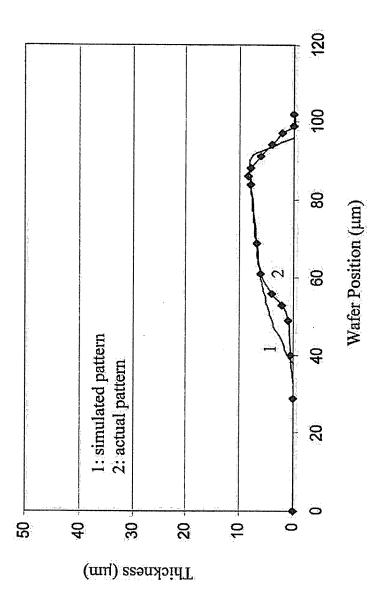
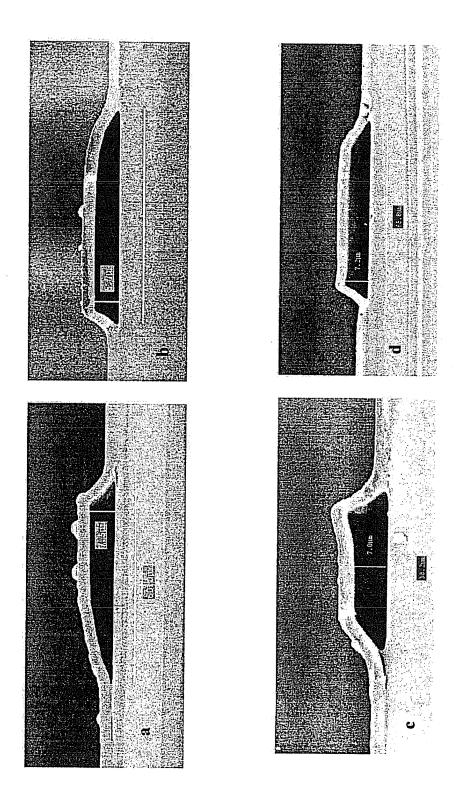
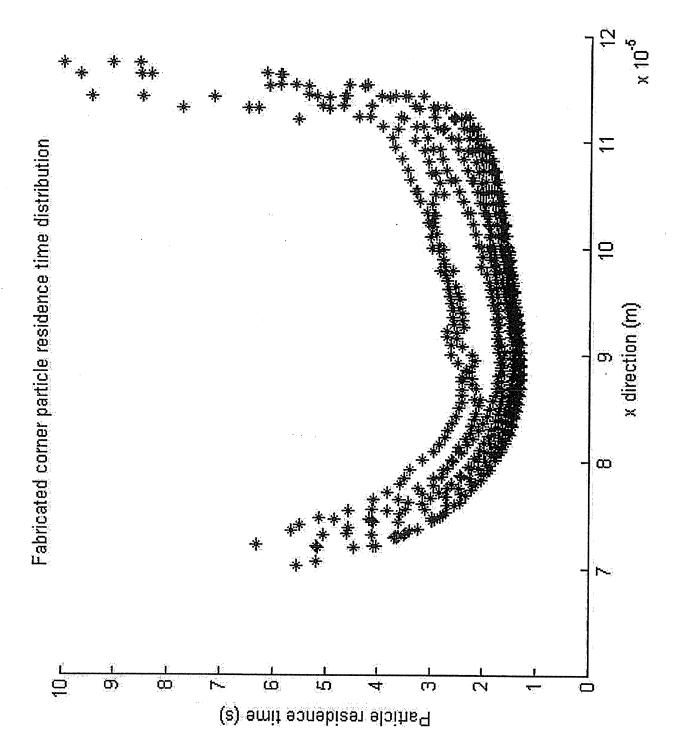


Figure 13





Microfluidic devices are becoming very important in several fields. The applications include rapid screening of drug synthesis, chemical synthesis, biological sensors, and microfuel cells, to name a few. In many applications, the devices involve flowing a fluid down a small channel. The applications often involve the analysis of a substance in the channel. A common problem occurs when the channel has a uniform height. For example, is a channel changes x/y direction (turns a corner), then the velocity of the fluid at the inner edge of the channel is greater than the furthest edge of the channel resulting in dispersion. At times, it would be desirable to have a region of the microfluidic device have a greater height so that a greater quantity of fluid will be present, such as for a chemical reactor.

A second improvement in this invention is the ability to use a photosensitive sacrificial polymer for the direct printing of microfluidic devices.

In this invention, we show that a photosensitive, sacrificial material is possible. We have demonstrated a negative tone, directly printable sacrificial polymer. The experiment below will serve as one example of how such a process may be carried out.

The sacrificial polymer is a co-polymer of 10 mole percent cyclol acrylate norbornene and 90 mole percent butyl norbornene. The polymer was dissolved in mesitylene to a final composition of 16 weight percent. Also added to the solution was 4 weight percent benzyl ethyl ether (BEE). The BEE is known to generate free radicals when exposed to ultra violet light. The free radicals can cross link the norbornene copolymer. The norbornene copolymer with BEE was spin coated onto a silicon wafer at 2000 to 4000 RPM and then soft baked at 90 to 110°C. The thin film of norbornene with BEE was then exposed to ultraviolet light using a lithography mask (patterns of light and dark). The exposed regions cross linked due to the free radicals generated by the BEE. The cross linked region became less soluble in a solvent. The unexposed regions were dissolved away by using an appropriate solvent, like xylene or bioact. The remaining pattern was then encapsulated with a dielectric material, like polyimide or silicon dioxide. After encapsulating, the sacrificial polymer was thermally decomposed leaving a buried air-cavity. Figure 1, 2 and 3 show SEM cross sections of the channels. Thus, the direct photoprinting of a microfluidic device is demonstrated.

The second aspect of this invention is the three-dimensional nature of the channels. Show contrast curves for the photo printing process. That is, the higher the optical exposure, the more polymer is left. The thicker the polymer-the higher the microfluidic channel. The edges of the channels in Fig. 1, 2 and 3 show tapered profiles. With the contrast curves, channels of arbitrary shape can be made.

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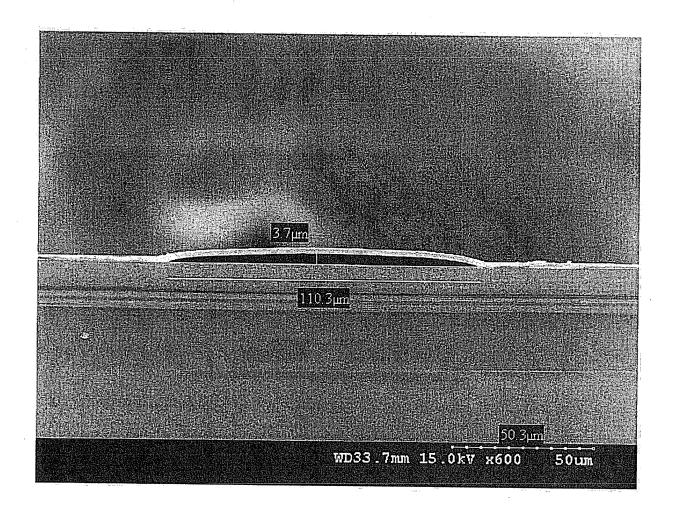


Fig. 1

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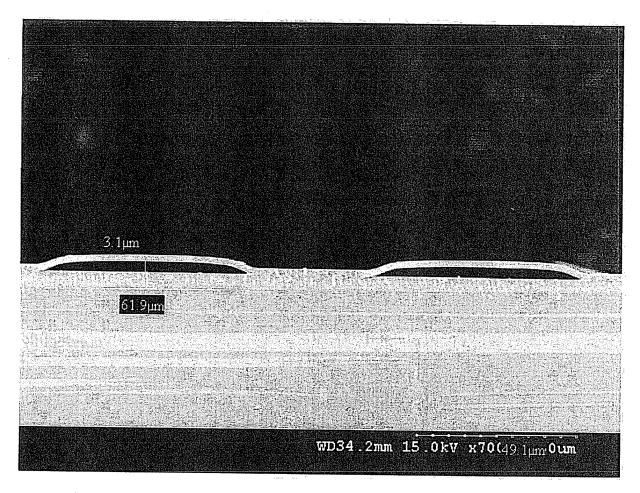
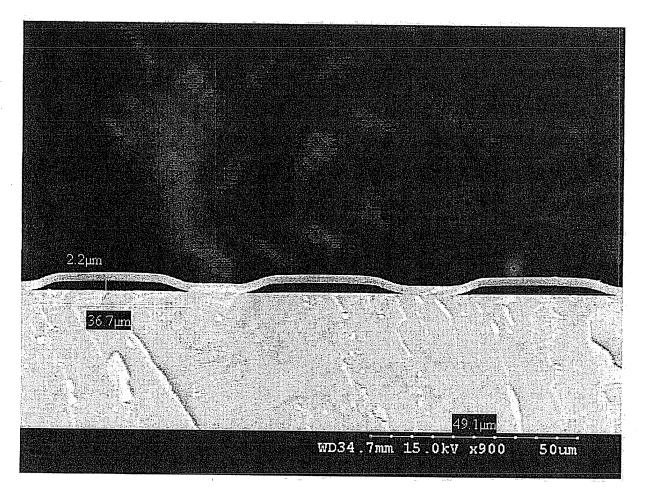


Fig. 2

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# Normalized Thickness vs Exposure Dose

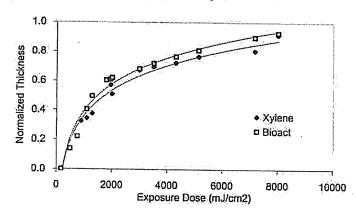
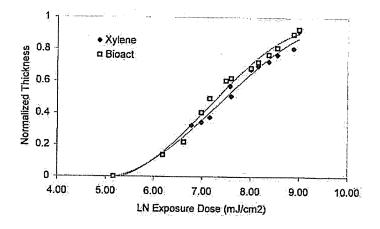


Fig. 4



Contrast Value: ~ 0.3

Fig. 5

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February 13, 2001

Dr. Paul Kohl Chemical Engineering Mail Code 0100

Dear Dr. Kohl:

We are writing to acknowledge receipt of the Invention Disclosure covering the invention entitled "Three-dimensional Microfluidic Device Fabrication". It is noted that your co-inventors are Sue Ann Bidstrup Allen, Clifford Lee Henderson and Xiaoqun Wu.

It is also noted that this invention was the result of sponsored research with NSF, GIT Project No. E-19-Y06.

For administrative purposes, we have assigned the identification number 2445 to the disclosure. Ms. Christi Kobatake, one of our Technology Licensing Associates, will be contacting you in the near future to discuss this invention disclosure with you.

Sincerely,

Evelyn Webb

Administrative Assistant

cc: Sue Ann Bidstrup Allen

Clifford Lee Henderson

Xiaoqun Wu

ID 2445

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